WHAT IS CLAIMED IS:

- A method for producing hyperbranched polymers, said method comprising the step of heating a polymerizable reaction charge comprising (a) a monomer mixture comprising (i) at least one monoethylenically unsaturated monomer in an amount of about 50-99.9% by weight of the monomer mixture and (ii) one or more multiethylenically unsaturated monomers in an amount of about 0.1-50% by weight of the monomer mixture, and (b) if at least one ethylenically unsaturated monomer of said monomer mixture is not a thermally initiating monomer, a free radical polymerization initiator, to a temperature in the range from about 250°C to about 400°C in a continuous reactor which allows mixing of the reactor contents for a residence time of from about 2 minutes to about 60 minutes, provided that if the total amount of multiethylenically unsaturated monomer is less than 3% by weight of the monomer mixture then at least one of said one or more multiethylenically unsaturated monomers must be tri- or greater ethylenically unsaturated.
- 2. The method of claim 1, wherein the multiethylenically unsaturated monomer is selected from the group consisting of diethylenically unsaturated monomers, triethylenically unsaturated monomers, tetraethylenically unsaturated monomers and mixtures thereof.
- 3. The method of claim 2, wherein the temperature is in the range from about 300°C to about 350°C.
- 4. The method of claim 3, wherein the continuous reactor is a continuous stirred tank reactor or a continuous loop reactor.

- 5. The method of claim 4, wherein the multiethylenically unsaturated monomer is divinylbenzene.
- 6. The method of claim 5, wherein the monoethylenically unsaturated monomer is styrene or a mixture of styrene and another monoethylenically unsaturated monomer.
- 7. The method of claim 6, wherein the other monoethylenically unsaturated monomer is selected from the group consisting of α -methylstyrene, acrylic acid, methacrylic acid, methyl methacrylate, butyl acrylate, butyl methacrylate, hydroxypropyl methacrylate and hydroxypropyl acrylate.
- 8. The method of claim 7, wherein the divinylbenzene is present in the monomer mixture in an amount in the range from about 10% by weight to about 15% by weight of the polymer.
- 9. The method of claim 8, wherein the residence time is from about 10 minutes to about 20 minutes.
- 10. The method of claim 9, wherein the reactor is substantially filled.
- 11. A hyperbranched polymer produced by the method comprising the step of heating a polymerizable reaction charge comprising (a) a monomer mixture comprising (i) at least one monoethylenically unsaturated monomer in an amount of 50-99.1% by weight of the monomer mixture and (ii) one or more multiethylenically unsaturated monomers in an amount of about 0.1-50% by weight of the monomer mixture, and (b) if at least one ethylenically unsaturated monomer mixture is not a thermally initiating monomer, a free radical polymerization

initiator, to a temperature in the range from about 250°C to about 400°C in a continuous reactor which allows mixing of the reactor contents for a residence time of from about 2 minutes to about 60 minutes, provided that if the total amount of multiethylenically unsaturated monomer is less than 3% by weight of the monomer mixture then at least one of said one or more multiethylenically unsaturated monomers must be tri- or greater ethylenically unsaturated.

- 12. The hyperbranched polymer of claim 11, wherein the multiethylenically unsaturated monomer is selected from the group consisting of diethylenically unsaturated monomers, triethylenically unsaturated monomers, tetraethylenically unsaturated monomers and mixtures thereof.
- 13. The hyperbranched polymer of claim 12, wherein the temperature is in the range from about 300°C to about 350°C.
- 14. The hyperbranched polymer of claim 13, wherein the continuous reactor is a continuous stirred tank reactor or a continuous loop reactor.
- 15. The hyperbranched polymer of claim 14, wherein the multiethylenically unsaturated monomer is divinylbenzene.
- 16. The hyperbranched polymer of claim 15, wherein the monoethylenically unsaturated monomer is styrene or a mixture of styrene and another monoethylenically unsaturated monomer.
- 17. The hyperbranched polymer of claim 16, wherein the other monoethylenically unsaturated monomer is selected from the group consisting of α -methylstyrene, acrylic

acid, methacrylic acid, methyl methacrylate, butyl acrylate, butyl methacrylate, hydroxyethyl methacrylate, hydroxypropyl methacrylate and hydroxypropyl acrylate.

- 18. The hyperbranched polymer of claim 17, wherein the divinylbenzene is present in the monomer mixture in an amount in the range from about 10% by weight to about 15% by weight of the polymer.
- 19. The hyperbranched polymer of claim 18, wherein the residence time is from about 10 minutes to about 20 minutes.
- 20. The hyperbranched polymer of claim 19, wherein the reactor is substantially filled.
- 21. A hyperbranched polymer comprising at least about 3% by weight of repeat units derived from divinylic monomers, about 50 to about 97% by weight of repeat units derived from monoethylenically unsaturated monomers and having a polydispersity of less than about 20.
- 22. The hyperbranched polymer of claim 19 with at least 6% by weight of repeat units derived from divinylic monomers.